



Changeover time for single and twin-screw extruders

<u>Christopher Thurber</u>, Hyunwoo Kim, Jin Wang, Bob Wrisley, Eric Marchbanks, and Xiaoyun Chen

SPE International Polyolefins Conference February 28, 2017

Minimizing changeover time in extrusion

- Material and time is wasted during formulation changes
- Efficient changeovers improve environment and bottom line
- Goal: understand and compare changeover time for single and twin-screw extruders

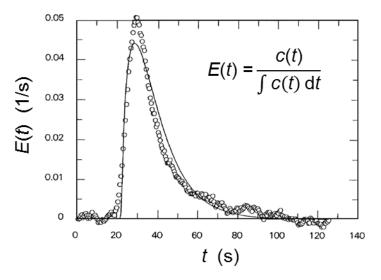


Operator: "Sometimes it takes days to purge out carbon black"

Residence time vs changeover time

Residence Time

- Time for a fluid element to pass through extruder at steady state
- Reactive extrusion, mixing
- Pulsed tracer experiment
- Many reports and well studied



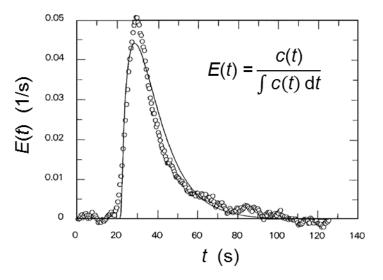
"Viscosity has little effect on twin screw extruder residence time"

Puaux et al, *Chem. Eng. Sci.*, 55: 1641 (**2000**); Poulesquen et al. *Polym. Eng. Sci.*, 43(12): 1841 (**2003**)

Residence time vs changeover time

Residence Time

- Time for a fluid element to pass through extruder at steady state
- Reactive extrusion, mixing
- Pulsed tracer experiment
- Many reports and well studied

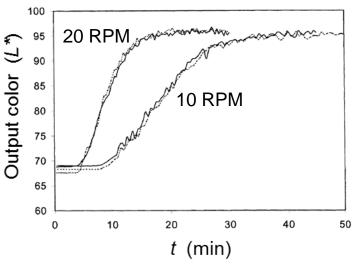


"Viscosity has little effect on twin screw extruder residence time"

Puaux et al, *Chem. Eng. Sci.*, 55: 1641 (**2000**); Poulesquen et al. *Polym. Eng. Sci.*, 43(12): 1841 (**2003**)

Changeover Time

- Time to change from one steady state to another, transient
- Product changeover, purging
- Industry experience but not many academic reports

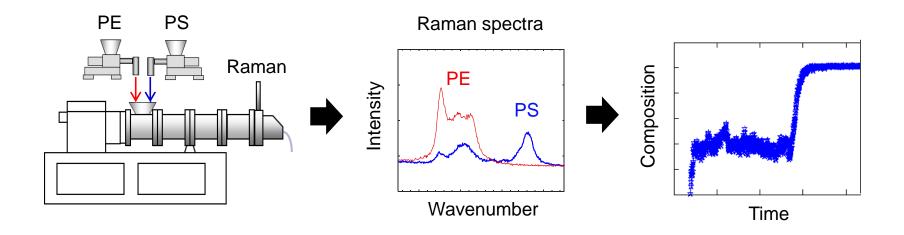


"Purging a high viscosity resin with low viscosity resin takes more time"

Gilmor et al., Polym. Eng. Sci., 43(2): 356 (2003)

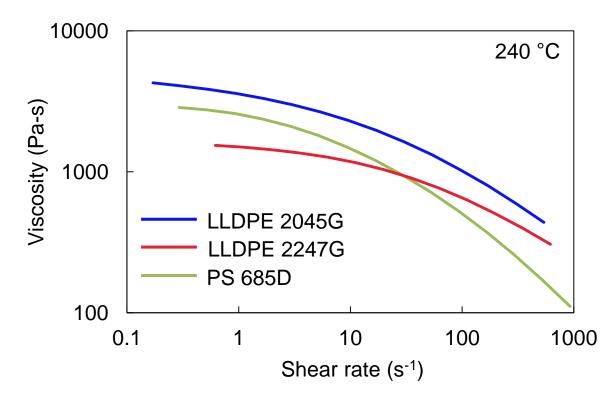
Online Raman spectroscopy for changeover time

- Switch polyethylene (PE) and polystyrene (PS) feed ratio
- Measure Raman spectra of extrudate over time
- Convert to composition time plots, extract changeover time



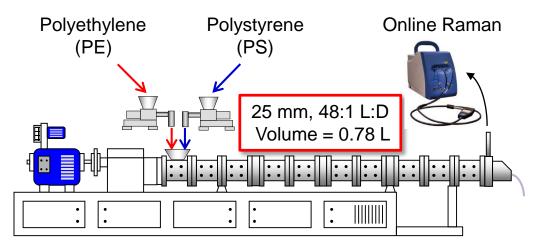
Materials

Name	Notation	MFI	Density (g/cm ³)	
DOWLEX [™] 2045G	LLDPE 2045G	1.0	0.920	
DOWLEX [™] 2247G	LLDPE 2247G	2.3	0.917	
Styron 685D	PS 685D	1.5	1.05	



Experimental setup

Twin-screw extruder setup

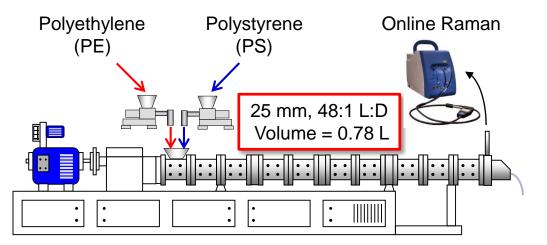


Wang et al., ANTEC Papers, 2016

- Mass flow rate (10, 20 lb/h)
- Viscosity ratio (1.0, 6.4 MI PE)
- Screw speed (400, 500 rpm)
- Mixing zone location (barrel 3 or 7)
- Composition change
 100/0 → 50/50 → 0/100 →
 50/50 → 100/0 (PE/PS wt%)

Experimental setup

Twin-screw extruder setup

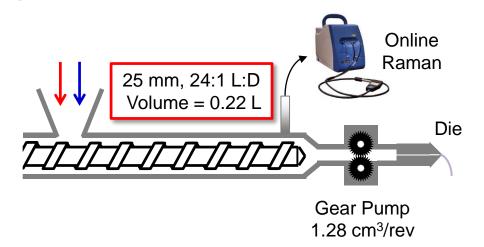


• Mass flow rate (10, 20 lb/h)

- Viscosity ratio (1.0, 6.4 MI PE)
- Screw speed (400, 500 rpm)
- Mixing zone location (barrel 3 or 7)
- Composition change
 100/0 → 50/50 → 0/100 →
 50/50 → 100/0 (PE/PS wt%)

Wang et al., ANTEC Papers, 2016

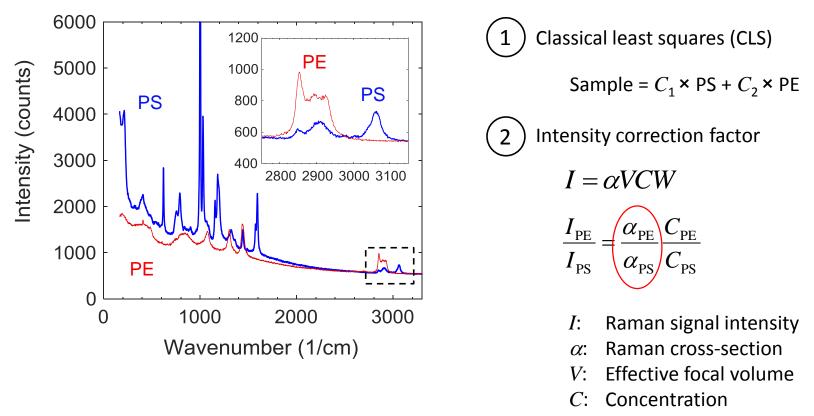
Single-screw extruder setup



- Mass flow rate (4, 10 lb/h)
- Viscosity ratio (1.0, 2.3 MI PE)
- Composition change
 100/0 → 50/50 → 0/100 →
 50/50 → 100/0 (PE/PS wt%)

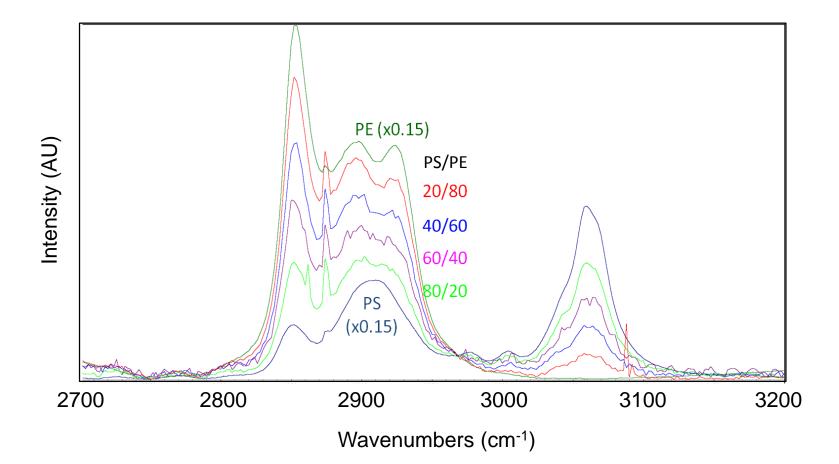
Accurate compositions from Raman spectra

- Classical least squares method (CLS)
- Fit a linear combination of pure PE and PS spectra to sample spectra
- Linear combination pre-factors are related to concentrations



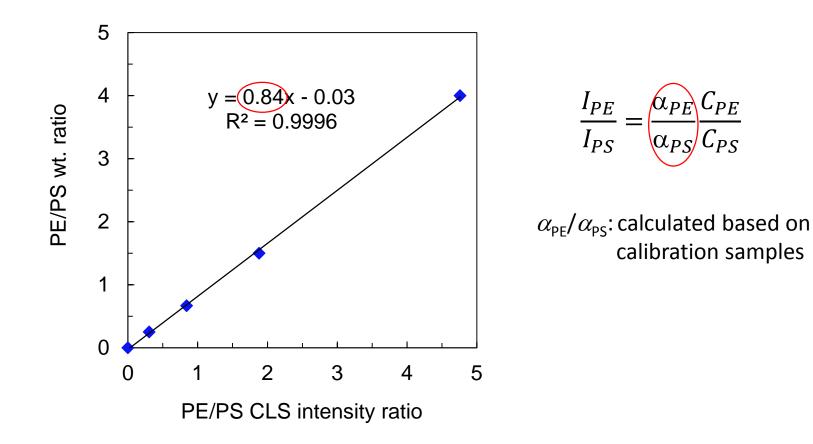
Raman calibration across range of compositions

- Correction term is necessary to account for melt transparency
- Online Raman spectra collected at a variety of steady-state compositions



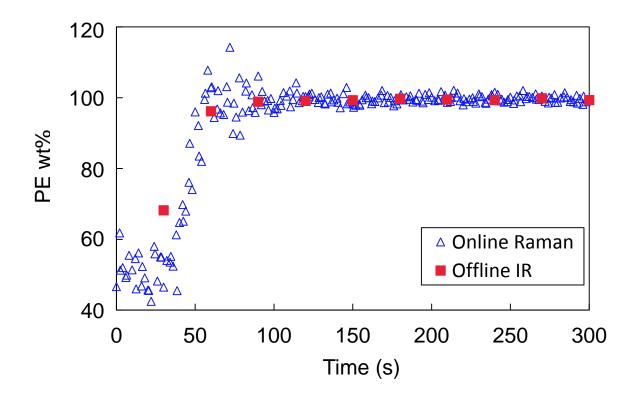
Quantitation from Raman signal

- Very good linear relationship between CLS intensity and concentration
- More accurate than visual observation of colorants



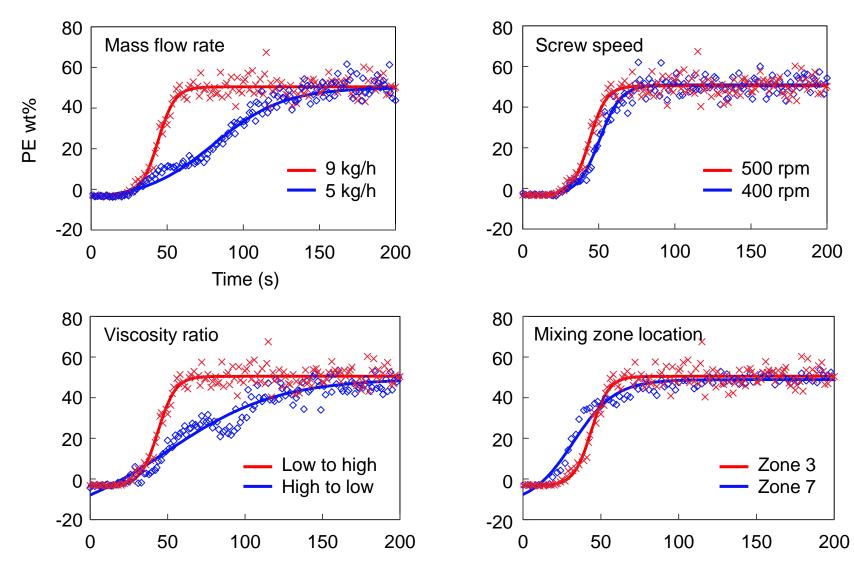
Online Raman method validation

- Collect extrudate sample every 30 s
- Measure the sample composition using offline ATR-FTIR
- Agreement with online Raman results



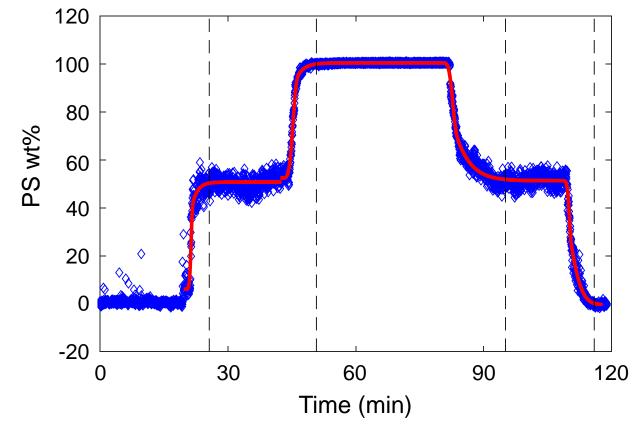
TSE, 4.5 kg/h, 500 rpm, LLDPE 2045G/PS 685D (50/50) \rightarrow 100% LLDPE 2045G Wang et al., ANTEC Papers, **2016**

TSE results: Changeover times 1 – 3 min



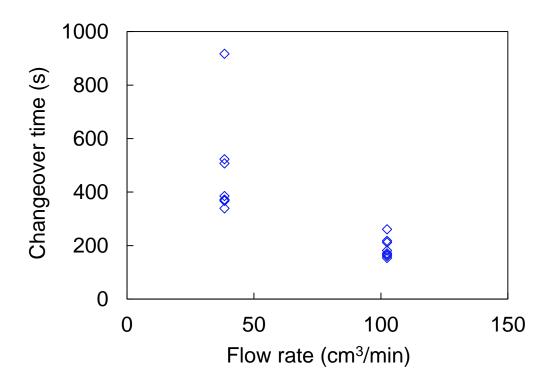
Single-screw extruder (SSE) experiments

- MATLAB online fitting and analysis
- Double Weibull curve fit to reduce noise
- Changeover time criteria: 99% of change complete



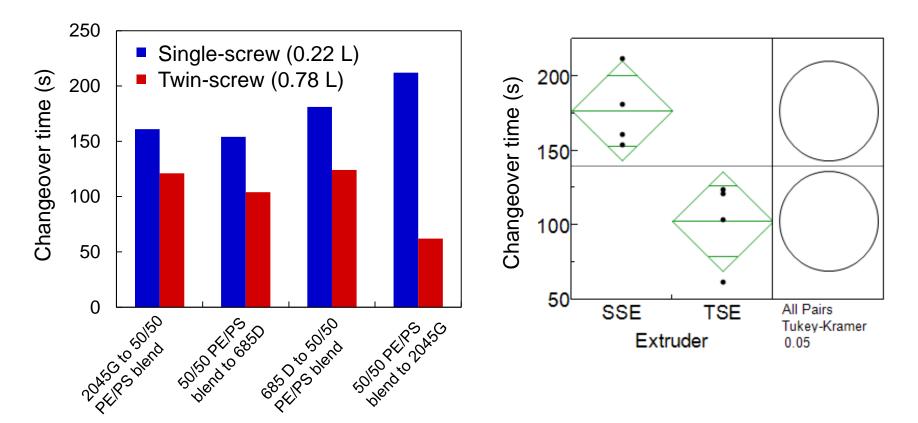
SSE results: Changeover times 2.5 – 15 min

- Increasing flow rate decreases changeover time
- Effects of viscosity ratio less pronounced, but weak, opposite effect of TSE
 - Stationary boundary layer (Kim et al., SPE Polyolefins, 2017)



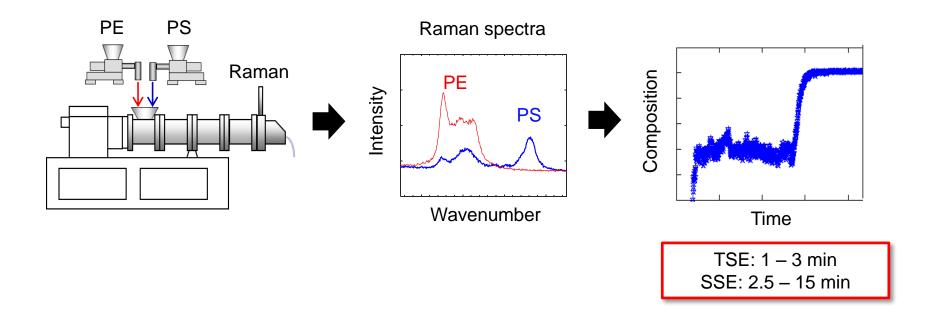
Comparison of changeover times

- Changeover times at same flow rate, materials
- TSE changeover is more rapid
- Hypothesis: self-wiping capability of TSE leads to shorter tail of distribution



Conclusions

- Increase throughput to decrease changeover time
- Online Raman exit composition validated
- TSE changes formulation more rapidly than SSE





Offline IR on Sample Composition

PE/PS blends prepared using Haake mixer for calibration

	Sample	Actual		CLS response		CLS predicted	
		PE	PS	CLS PE	CLS PS	PE	PS
						100.00	
	1	100%	0%	1	0	%	0.00%
	2	95%	5%	1.721	0.080	95.27%	4.73%
	3	90%	10%	1.240	0.117	90.84%	9.16%
	4	50%	50%	0.489	0.458	49.89%	50.11%
	5	10%	90%	0.178	1.334	11.04%	88.96%
	6	5%	95%	0.083	0.908	7.84%	92.16%
							100.00
Absorbance	0.55- 0.50- 0.45- 0.40- 0.35- 0.30- 0.25- 0.20- 0.15- 0.10- 0.05- 0.00- 850	900 95	0 1000	1050 1100 Waterumbers	50	0/10 PE/PS 0/50 PE/PS 0/90 PE/PS	PE PS 1550 1400

